

+135-3858-6433 (GuangDong)  
+188-1699-6168 (ShangHai)  
+852-6957-5415 (HongKong)

release 09/1998

# Injection Moulding

## *mini guide*



Contents

update ►





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***GE Plastics***

# Injection Moulding

## *mini guide*

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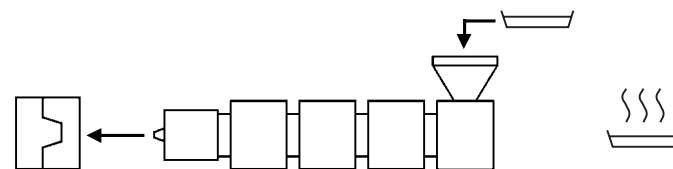
Profile

<b>Cyclocac®</b>		AFR450B	62	BST44	73	261R	19	V180HF	33	310SEO	76
<b>ABS</b>		AFR450X1	64	BS6	70	263R	19	V190	40	312C	76
CRT3370	2	AFR450X2	64	BS10	70	2814R	17	725A	29	315	76
EP	3	AFR460B	62	BT6	69	3412R	17	731(S)	29	325(C)(F)	76
GPM5500	1	AFR470X1	64	B28(H)(N)	74	3413R	17			325M	76
GPM5500M	1	AFR470X2	64	B28(U)(UL)	74	3431R	17	<b>Noryl GTX®</b>		357X	76
GPM5500S	1	AFR560B	62	B40	74	500R	17	<b>PPE/PA</b>		359	76
GPM5500T	1	AFR682A1	65	CFR200Y	75	503R	17	GTx810	41	3607U	76
GSM	7	AG3(K)	61			920(A)	18	GTx820	41	362	76
G121	1	AG4(K)	61	<b>Lexan®</b>		923(A)	18	GTx830	41	4012	76
G320	7	AG5(K)	61	<b>PC</b>		940(A)	18	GTx914	42	4022	76
G360	9	AG6(K)	61	FL900P	23	943(A)	18	GTx918W	42	4031	76
G361	9	AG6ST01	61	GR1210	23	950(A)	19	GTx924	43	4032	76
G365	9	AG6ST43	61	HF1110R	18	953A	19	GTx934	43	412	76
G366(M)	9	AG7(K)	61	HF1130R	18			GTx944	43	420(SEO)	76
G368	7	AG10(K)	61	HF1140R	18	<b>Noryl®</b>		GTx954	43	430	76
SEA2	5	AK6	66	HF500R	18	<b>PPE/PS</b>		GTx964	43	451E	76
S157	5	AK8	66	LS1	18	CTI2550	29	GTx974	43	4521	76
S570	1	ALM	67	LS2	19	FN150	33			457	76
S700(S)(T)	1	ALY540A	67	LS3	17	GFN1(V)	29	<b>Ultem®</b>		4631	76
S701(S)	1	ALY640A1	68	ML3019	17	GFN1720	30	<b>PEI</b>		467	76
S702(S)	1	AST02	67	ML3041	18	GFN2(V)	29	AR9300	53	5021	76
S703	3	AST03	67	ML3042	17	GFN3(V)	31	ATX100F	83	5031	76
S704(S)	1	AST04	67	ML3260	19	HB1525	32	ATX200F	84	508	76
S705	3	AST41	67	ML3286	17	HB3525	29	CRS5001	54	5510	76
S706(S)	1	AST43	67	ML3400	19	HF180	33	CRS5201	50	553	76
VW300	6	AST44	67	ML3513	17	HF185	33	CRS5311	50	735	57
VW55(M)	5	AS6	61	ML3562	19	HIN120P	29	1000	47	7523	76
XS158M	5	A28(K)(N)	67	ML3729	18	IN120	29	1010	47	771	79
X37	9	A28UL	67	OQ1020LN	25	N110(S)	34	1010F	48	8032(U)	57
		BFR200A	69	OQ1030LN	25	N110HG	34	1110(F)	49	815	57
<b>Cyclocoloy®</b>		BFR200Y	69	OQ3620	17	N190	33	2100	47	830	57
<b>PC/ABS</b>		BFR450A	70	OQ2830	17	PX1112(A)	29	2110	47	855	57
C1000(A)	11	BFR450B	70	OQ4320	19	PX1115	29	2200	48	865	57
C1000HF	11	BFR460A	70	OQ4820	17	PX1134	29	2210	48		
C1100(A)	12	BFR552Y3	70	101(R)	17	PX1180	36	2300	48	<b>Xenoy®</b>	
C1100HF	12	BGS6H1	70	103(R)	17	PX1181	36	2310	48	<b>PC/PBT</b>	
C1200(HF)	13	BG3(H)	71	104R	17	PX1185	36	2312	49	CL100B	79
C1200HF13	13	BG4(H)	71	121(R)	18	PX1786G	37	2400	50	CL101	79
C2100HF	14	BG5(H)	71	123R	18	PX2245	33	2410	50	CL200	79
C2800	15	BG6(H)(U)	71	124R	18	PX9406N	29	4000	51	CL300	79
C2950	14	BG6ST02	69	1278R	19	SE0	29	4001	47	CL500U	79
C6200	15	BG6ST41	69	134R	17	SE1	29	6000	50	XL1339	81
C6400	15	BG6ST43	69	141(R)	19	SE90	33	7801	50	XL1562	79
LG9000	12	BG10(H)	71	143(R)	19	SE100	29	9075	52	1760T	80
		BG7(H)	71	144R	19	SE1GFN1	29			5730	79
<b>Enduran®</b>		BG8	71	161R	19	SE1GFN2	29	<b>Valox®</b>		6370	80
<b>PBT</b>		BK8	72	163R	19	SE1GFN3	37	<b>PBT-PET</b>		6380U	82
7062(X)	78	BLM	73	164(R)	19	V0150B	37	DR48	76		
		BPP01	73	201R	17	V01505	36	DR51	76		
<b>Gelon™</b>		BST01	73	2014R	19	V01525	29	VAC3001N	76		
<b>PA6.6/PA6</b>		BST02	73	2034	19	V01550	37	VX5005	76		
ACF6	61	BST03	73	221R	18	V02570	30	VX5011	76		
AFG6	61	BST04	73	223R	18	V03505	29	VX5022	76		
AFD900R	62	BST42	73	241(R)	19	V03550	38	260HPR	76		
	63	BST43	73	243R	19	V090	39	3007	76		



October  
1999

October  
1998



Mould	Melt temp.	Nozzle	Zone 3	Zone 2	Zone 1	Hopper	Moisture content	Predrying			Profile
°C	°C	°C	°C	°C	°C	°C	% max.	Hours	°C	▼	
40-80	220-260	210-250	220-260	220-260	200-240	60-80	0.1	2-4	85-95	1	
40-80	230-260	220-250	230-260	230-260	220-250	60-80	0.1	2-4	85-95	2	
65-80	250-270	240-260	245-265	240-260	230-250	60-80	0.05	2-4	85-95	3	
40-80	200-230	190-220	195-225	195-225	180-210	60-80	0.1	2-4	80-85	5	
40-80	180-210	180-200	185-205	185-205	170-190	60-80	0.1	2-4	80-85	6	
40-80	240-270	220-260	230-270	210-250	210-250	60-80	0.1	2-4	85-95	7	
40-80	250-280	245-275	250-280	250-280	230-260	60-80	0.1	2-4	90-100	9	
60-90	240-270	220-260	230-270	230-270	210-240	60-80	0.02	2-4	90-100	11	
60-90	250-280	230-270	240-280	240-280	220-250	60-80	0.02	2-4	95-105	12	
60-90	260-290	240-280	250-290	250-290	230-260	60-80	0.02	2-4	100-110	13	
60-90	250-280	230-270	240-280	230-270	210-240	60-80	0.02	2-4	90-100	14	
50-70	230-270	220-260	230-270	220-260	200-230	60-80	0.02	2-4	80-90	15	
80-120	290-320	280-310	290-320	280-310	270-300	60-80	0.02	2-4	120	17	
80-100	280-300	270-290	280-300	270-290	260-280	60-80	0.02	2-4	120	18	
80-110	280-310	270-290	280-310	270-290	260-280	60-80	0.02	2-4	120	19	
65-95	290-320	290-320	290-320	280-310	265-295	60-80	0.02	2-4	120	23	
80-100	300-330	280-320	300-340	280-320	240-280	60-80	0.02	4-6	120	25	
80-120	280-300	260-280	280-300	260-280	240-260	60-80	-	2-3	100-120	29	
80-120	290-330	290-310	310-330	290-310	270-290	60-80	-	2-4	110-120	30	
80-120	280-300	280-300	290-310	270-290	250-270	60-80	-	2-4	100-120	31	
80-100	280-300	270-290	280-300	260-280	240-260	60-80	-	2-3	100-110	32	
60-80	260-280	240-260	260-280	240-260	220-240	60-80	-	2-3	80-100	33	
60-100	280-300	260-280	280-300	260-280	240-260	60-80	-	2-4	80-100	34	
60-100	280-300	260-280	280-300	260-280	240-260	60-80	-	2-3	80-100	36	
100-130	300-320	280-300	300-320	280-300	260-280	80-100	-	2-3	110-120	37	
100-130	280-310	280-300	300-320	280-300	260-280	80-100	-	2-4	110-120	38	
60-80	270-290	250-270	270-290	250-270	230-250	60-80	-	2-3	70-80	39	
60-80	260-280	240-260	260-280	240-260	220-240	60-80	-	2-4	80-100	40	
80-100	280-300	270-290	280-300	270-290	260-280	60-80	0.02	2-3	100-110	41	
80-120	280-310	270-300	280-300	270-290	260-280	60-80	0.02	2-3	100-120	42	
80-120	290-320	280-310	290-320	280-300	260-280	60-80	0.02	2-3	100-120	43	
140-180	370-410	350-405	360-415	350-405	340-395	80-120	0.02	4-6	150	47	
140-180	370-410	360-410	370-420	360-410	350-400	80-120	0.02	4-6	150	48	
140-180	360-400	360-400	370-410	360-400	240-380	80-100	0.02	4-6	150	49	
140-180	370-410	370-410	380-420	370-410	350-390	80-100	0.02	4-6	150	50	
140-180	370-415	360-405	370-415	360-405	350-395	80-120	0.02	4-6	150	51	
140-160	360-380	360-380	360-380	345-365	320-340	80-120	0.02	4-6	160	52	
135-140	350-400	350-410	350-410	350-400	350-370	80-120	0.02	4-6	150	53	
120-170	360-410	360-400	370-410	350-390	325-365	80-120	0.02	4-6	150	54	

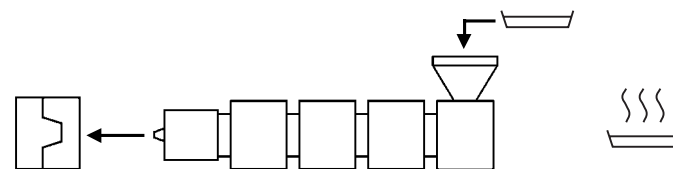
Temperature Profiles are only guidelines, to be used for start-up. Drying times as mentioned are 'hot residence times' (pellets are at drying temperature) resulting in low moisture levels as indicated. Excessive drying times should be avoided. Please check with your local GE Plastics' representative to ensure you have the most up-to-date information.

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Profile

<b>Cyclocac®</b>		AFR450B	62	BST44	73	261R	19	V180HF	33	310SEO	76
<b>ABS</b>		AFR450X1	64	BS6	70	263R	19	V190	40	312C	76
CRT3370	2	AFR450X2	64	BS10	70	2814R	17	725A	29	315	76
EP	3	AFR460B	62	BT6	69	3412R	17	731(S)	29	325(C)(F)	76
GPM5500	1	AFR470X1	64	B28(H)(N)	74	3413R	17			325M	76
GPM5500M	1	AFR470X2	64	B28(U)(UL)	74	3431R	17	<b>Noryl GTX®</b>		357X	76
GPM5500S	1	AFR560B	62	B40	74	500R	17	<b>PPE/PA</b>		359	76
GPM5500T	1	AFR682A1	65	CFR200Y	75	503R	17	GTx810	41	3607U	76
GSM	7	AG3(K)	61			920(A)	18	GTx820	41	362	76
G121	1	AG4(K)	61	<b>Lexan®</b>		923(A)	18	GTx830	41	4012	76
G320	7	AG5(K)	61	<b>PC</b>		940(A)	18	GTx914	42	4022	76
G360	9	AG6(K)	61	FL900P	23	943(A)	18	GTx918W	42	4031	76
G361	9	AG6ST01	61	GR1210	23	950(A)	19	GTx924	43	4032	76
G365	9	AG6ST43	61	HF1110R	18	953A	19	GTx934	43	412	76
G366(M)	9	AG7(K)	61	HF1130R	18			GTx944	43	420(SEO)	76
G368	7	AG10(K)	61	HF1140R	18	<b>Noryl®</b>		GTx954	43	430	76
SEA2	5	AK6	66	HF500R	18	<b>PPE/PS</b>		GTx964	43	451E	76
S157	5	AK8	66	LS1	18	CTI2550	29	GTx974	43	4521	76
S570	1	ALM	67	LS2	19	FN150	33			457	76
S700(S)(T)	1	ALY540A	67	LS3	17	GFN1(V)	29	<b>Ultem®</b>		4631	76
S701(S)	1	ALY640A1	68	ML3019	17	GFN1720	30	<b>PEI</b>		467	76
S702(S)	1	AST02	67	ML3041	18	GFN2(V)	29	AR9300	53	5021	76
S703	3	AST03	67	ML3042	17	GFN3(V)	31	ATX100F	83	5031	76
S704(S)	1	AST04	67	ML3260	19	HB1525	32	ATX200F	84	508	76
S705	3	AST41	67	ML3286	17	HB3525	29	CRS5001	54	5510	76
S706(S)	1	AST43	67	ML3400	19	HF180	33	CRS5201	50	553	76
VW300	6	AST44	67	ML3513	17	HF185	33	CRS5311	50	735	57
VW55(M)	5	AS6	61	ML3562	19	HIN120P	29	1000	47	7523	76
XS158M	5	A28(K)(N)	67	ML3729	18	IN120	29	1010	47	771	79
X37	9	A28UL	67	QQ1020LN	25	N110(S)	34	1010F	48	8032(U)	57
		BFR200A	69	QQ1030LN	25	N110HG	34	1110(F)	49	815	57
<b>Cycloley®</b>		BFR200Y	69	QQ3620	17	N190	33	2100	47	830	57
<b>PC/ABS</b>		BFR450A	70	QQ2830	17	PX1112(A)	29	2110	47	855	57
C1000(A)	11	BFR450B	70	QQ4320	19	PX1115	29	2200	48	865	57
C1000HF	11	BFR460A	70	QQ4820	17	PX1134	29	2210	48		
C1100(A)	12	BFR552Y3	70	101(R)	17	PX1180	36	2300	48		
C1100HF	12	BGS6H1	70	103(R)	17	PX1181	36	2310	48		
C1200(HF)	13	BG3(H)	71	104R	17	PX1185	36	2312	49	CL100B	79
C1200HFM	13	BG4(H)	71	121(R)	18	PX1786G	37	2400	50	CL101	79
C2100HF	14	BG5(H)	71	123R	18	PX2245	33	2410	50	CL200	79
C2800	15	BG6(H)(U)	71	124R	18	PX9406N	29	4000	51	CL300	79
C2950	14	BG6ST02	69	1278R	19	SE0	29	4001	47	CL500U	79
C6200	15	BG6ST41	69	134R	17	SE1	29	6000	50	XL1339	81
C6400	15	BG6ST43	69	141(R)	19	SE90	33	7801	50	XL1562	79
LG9000	12	BG10(H)	71	143(R)	19	SE100	29	9075	52	1760T	80
		BG7(H)	71	144R	19	SE1GFN1	29			5730	79
<b>Enduran®</b>		BG8	71	161R	19	SE1GFN2	29	<b>Valox®</b>		6370	80
<b>PBT</b>		BK8	72	163R	19	SE1GFN3	37	<b>PBT - PET</b>		6380U	82
7062(X)	78	BLM	73	164(R)	19	V0150B	37	DR48	76		
		BPP01	73	201R	17	V01505	36	DR51	76		
<b>Gelon™</b>		BST01	73	2014R	19	V01525	29	VAC3001N	76		
<b>PA6.6/PA6</b>		BST02	73	2034	19	V01550	37	VX5005	76		
ACF6	61	BST03	73	221R	18	V02570	30	VX5011	76		
AFG6	61	BST04	73	223R	18	V03505	29	VX5022	76		
AFD9000	62	BST42	73	241(R)	19	V03550	38	260HPR	76		
	63	BST43	73	243R	19	V090	39	3007	76		

October  
1998



Mould	Melt temp.	Nozzle	Zone 3	Zone 2	Zone 1	Hopper	Moisture content	Predrying	Profile
°C	°C	°C	°C	°C	°C	°C	% max.	Hours	°C
60-110	260-285	265-275	260-280	255-280	240-260	40-60	0.02	4-6	110-120
70-120	260-290	250-270	260-280	260-280	270-290	60-80	0.2	4-6	75-85
70-100	260-280	250-270	260-280	260-280	270-290	60-80	0.2	4-6	75-85
40-80	260-280	250-270	260-280	260-280	260-280	60-80	0.2	4-6	75-85
90-120	260-290	260-280	270-290	270-290	270-290	60-80	0.2	4-6	75-85
80-100	260-280	250-270	260-280	260-280	260-280	60-80	0.2	4-6	75-85
90-110	270-290	260-280	270-290	270-290	270-290	60-80	0.2	4-6	75-85
70-90	260-280	250-270	260-280	260-280	260-280	60-80	0.2	4-6	75-85
70-90	260-290	260-280	270-290	270-290	270-290	60-80	0.2	4-6	75-85
60-80	240-260	230-250	240-260	240-260	240-260	60-80	0.2	4-6	75-85
70-90	250-270	240-260	250-270	250-270	250-270	60-80	0.2	4-6	75-85
70-120	250-280	240-270	250-280	250-280	250-280	60-80	0.2	4-6	75-85
70-100	260-280	250-270	260-280	260-280	260-280	60-80	0.2	4-6	75-85
60-90	220-250	210-240	220-250	220-250	220-250	60-80	0.2	4-6	75-85
60-80	220-240	210-230	220-240	220-240	220-240	60-80	0.2	4-6	75-85
70-90	240-260	230-250	240-260	240-260	240-260	60-80	0.2	4-6	75-85
40-100	250-270	240-260	245-265	240-255	230-245	40-60	0.02	2-4	110-120
60-100	255-280	245-270	250-270	240-260	230-250	40-60	0.02	2-4	110-120
60-80	255-270	250-265	250-270	240-265	230-250	40-60	0.02	2-4	90-100
60-100	255-270	250-265	250-270	240-265	230-250	40-60	0.02	2-4	100-110
60-100	265-275	260-275	260-280	250-275	240-270	60-80	0.02	4-6	110-120
60-110	265-285	260-275	260-280	250-275	240-270	60-80	0.02	4-6	110-120
100-125	325-360	320-340	320-340	310-330	300-320	60-80	0.02	3-4	125-135
125-140	340-380	340-360	340-360	330-350	320-340	80-100	0.02	3-4	130-140

Temperature Profiles are only guidelines, to be used for start-up. Drying times as mentioned are 'hot residence times' (pellets are at drying temperature) resulting in low moisture levels as indicated. Excessive drying times should be avoided. Please check with your local GE Plastics' representative to ensure you have the most up-to-date information.

# Product overview

This Injection Moulding mini guide – supplementary to the Injection Moulding brochure that shows detailed information – is specially designed as a handy pocket guide and quick reference for use on the shop floor. The inlaid pages show details on pre-drying and temperature settings of machine, mould and material for all standard GE Plastics' resins.

## 1.1 Amorphous injection moulding resins

Cycolac®	<i>ABS Resins</i>
Cycoloy®	<i>PC+ABS Thermoplastic Alloys</i>
Lexan®	<i>PC Polycarbonate Resins</i>
Noryl®	<i>PPE+PS Modified PPO® Resins</i>
Noryl®Xtra	<i>PPE+PS Modified PPO® Resins</i>
Ultem®	<i>PEI Polyetherimide Resins</i>

## 1.2 Semi-crystalline injection moulding resins

Enduran®	<i>PBT Thermoplastic Polyester Resins</i>
Lomod®	<i>Flexible Engineering Thermoplastic Resins</i>
Noryl GTX®	<i>PPE Modified PA Alloys</i>
Supec®	<i>PPS Polyphenylenesulphide Resins</i>
Valox®	<i>PBT+PET Thermoplastic Polyester Resins</i>
Xenoy®	<i>PC+PBT Thermoplastic Alloys</i>

## 1.3 Other products

Azdel® - Azloy® -	
Azmet®	<i>Technopolymer Structures</i>
Remex™	<i>Engineering Plastics</i>
Kapronet®	<i>Purging Compound</i>



# Materials

## 2.1 Storage

GE Plastics' resins are supplied in the form of ready-to-process pellets in sealed bags or containers. No special storage conditions are necessary, however, all containers must be kept dry and away from sunlight since UV radiation could affect both packaging and contents. Special care must be taken to keep Lexan and Noryl GTX resins as dry as possible during storage.

## 2.2 When can resin pick up moisture?

- during transport and storage
- during prolonged exposure to atmosphere, even after initial drying
- on its way to the machine hopper, when no hot (dry) air is used
- in case of high relative humidity

## 2.3 When can moisture be a problem?

- pellets packed too deeply in the trays of drying ovens: lack of air circulation will prevent drying
- inefficient drying equipment
- machine hopper lid not sealed

## 2.4 Importance of pre-drying

Most thermoplastics absorb atmospheric moisture, which under normal processing conditions can cause degradation of the polymer. Specially Lexan, Ultem and Valox as hygroscopic resins demand proper pre-drying before moulding: these polymers do react with moisture at high (processing) temperatures. When this reaction occurs, polymer chains break, resulting in loss of properties. Excessive moisture can manifest itself in splay, silver streaking, blisters or degradation, which reduce the cosmetic and physical properties of moulded components. The removal of moisture is therefore essential to ensure optimal performance of the finished part. Although Noryl resin has one of the lowest moisture

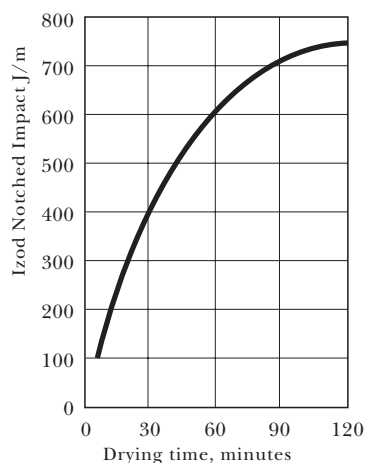




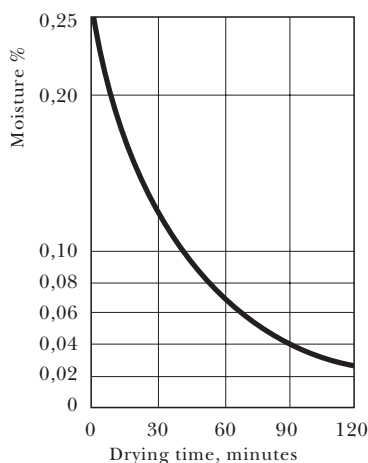
## 2.3 Pre-drying times

absorption levels of engineering plastics, it is advised to dry before moulding - particularly where surface appearance is critical. For **filled materials** the drying time might be slightly longer; the allowed moisture level is the same. Due to a larger surface area of the pellets, **recycled resins** have a faster pick-up rate of moisture: drying time should in general be increased from 4 to 6 hours. It is recommended to dry regrind materials separately.

Effect of drying time  
on impact strength of  
**Lexan resin**



Effect of drying time  
on moisture content of  
**Lexan resin, at 120°C**

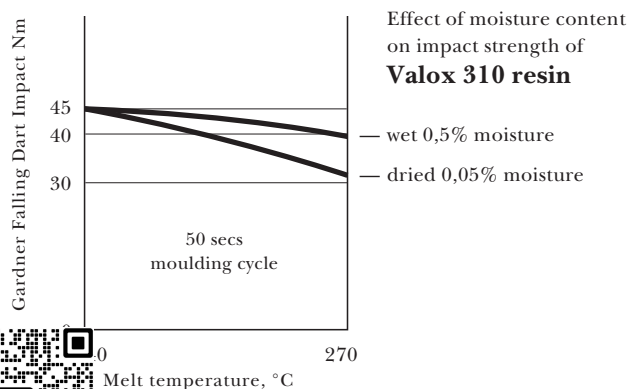


Although exceeding recommended drying times will not affect the properties of resins such as Lexan, Valox, Ultem and Xenoy, it is recommended not to dry for longer periods of time as indicated in the enclosed inlay.

With Noryl resin, exceeding drying times may result in surface defects due to oxidization. 90% of Noryl resin's moisture is removed anyway during the first hour of drying. Excessive drying time with Cyclocac resin may give a slight surface oxidation of the pellets resulting in colour shift of light colours. This is caused by the fact that too long or too high air temperature may drive out required additives: resin will process poorly, parts get brittle, colours change.

It is important that the typical drying times assume that the pellets are up to drying temperature 'before the clock starts'. Drying time taken to get the pellets up to drying temperature does not practically contribute to the effective overall drying.

For details per grade, see enclosed inlay.



## 2.6 TVI test for checking moisture content

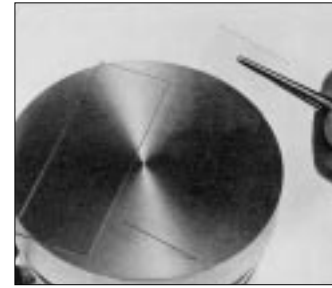
Measuring moisture content can be done by laboratory equipment such as the Carl Fischer titration method or others. Since these long, unwieldy lab techniques are impractical in most moulding shops, GE Plastics has developed a simple, fast and low-cost method to determine whether moisture-sensitive thermoplastic pellets are dry and ready for processing. In brief, this method means heating a few pellets to their melting point and observing whether bubbles are present (indicating moisture in the resin) or absent (indicating a dry material).

Called TVI (Tomasetti's Volatile Indicator), the test requires little in the way of equipment and calls for just four simple steps. See pictures.

The TVI test can be used for Lexan, Ultem, Noryl, Noryl GTX, Cyclocac, Cycology, Valox and Xenoy resins, but not for glass reinforced grades. Not to be used for Supec and Lomod resins.

The necessary equipment is a hot plate capable of maintaining various temperatures from 200 to 350°C, two glass microscope slides, a straight edge or tongue depressor, a pair of tweezers and ideally a surface pyrometer to check the plate temperature – if no hot plate is available, a quick check can be done by using a heater band of the moulding machine. Moisture is denoted by bubbles in the flattened granules: the number and size increase with the amount of moisture present.

A few small bubbles mean moisture contents of 0.02 to 0.03%, numerous bubbles indicate 0.05 to 0.1%, and many large bubbles moisture above 0.1%. To avoid misleading conclusions, it is advisable to always test at least four granules, as bubbles that appear in only some granules might be trapped air, rather than moisture.



PICTURE 1

Heat two microscope glass slides on hot plate for about two minutes (be sure surface is clean)- Valox and Xenoy resins: 250°C, Noryl and Noryl GTX resins: 280°C, Lexan resin: 290°C, Ultem resin: 350°C, Cyclocac resin: 250°C, Cycology resin: 275°C.



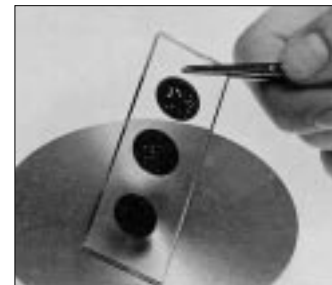
PICTURE 2

Use tweezers to place three or four pellets from the drier on one of the slides. Place the other slide immediately on top of the granules.



PICTURE 3

Press the two slides together with a straight edge until the granules are flattened out to about 12 mm diameter.



PICTURE 4

Remove the sandwiched slides and allow to cool. Amount and size of bubbles indicate percentage of moisture. If only one or two bubbles are present, they may be only trapped air and no moisture: to be sure, use at least three or four pellets.

# Injection moulding machine

## 3.1 Choosing a machine

### Shot size %

- shot size % - in general 30 to 90%, depending on resin type and in relation to residence time and melt temperature
- shot size < 20 % - can cause material degradation, part defects
- shot size > 90% - no melt homogeneity, inconsistent part quality, packing problems

### Residence time

- residence time - always related to melt temperature
- residence time - maximum 6 to 12 min. depending on resin type
- too long - material degradation
- too short - insufficient plastification and homogeneity of plasticized material
- colour pigments - high residence times may change colours



### 3.2 Screw geometry and design

#### L/D ratio and compression ratio

- L/D 22:1 to 25:1 - for Valox, Xenoy resins
- L/D 18:1 to 24:1 - for all other resins
- CR 2:1 to 2.5:1 - for all resins
- CR's higher than 2.5:1 - not recommended

#### Non-return valves / back flow valves

- sliding ring valves - for all resins
- ball check valves - not recommended

#### Nozzles

- open nozzles - for all resins
- reversed taper nozzles - for Cycolac resin, not for Valox resin
- shut-off nozzles - for Supec resin, not advised for other resins
- nozzle orifices - as large as possible, 1 mm smaller than sprue top
- nozzle temperature - heater band plus adequate control
- drooling - check nozzle radius

#### Screw cushion

- screw cushions - 3 to 10 mm of plasticizing stroke, dependent on screw diameter/ material compression

#### Screw speeds

- r.p.m. - always in relation to screw diameter
- circumferential speed - most important
- circumferential speed - unfilled and filled grades preferred 0.10 - 0.25 m/s.
- circumferential speed - grades with special fillers preferred 0.10 - 0.20 m/s.
- r.p.m. - adjust moulding cycle: screw rotation must fall in cooling time
- r.p.m. - as low as practicable, but beware of insufficient plastification

- too high r.p.m. - material degradation
- too high r.p.m. - breakage of glass fibres in glass filled products
- too high r.p.m. - increased wear of screw and barrel
- too high r.p.m. - inability to control melt temperature

### 3.3 Vented barrels

#### Do's

- do monitor carefully the temperature profile of the barrel
- do keep residence times below 8 min.
- do contact your local GE Plastics' representative for any advice on vented barrel processing

#### Don'ts

- don't process Ultem, Supec, Xenoy or Lomod resins using vented barrel equipment
- don't process FR grades using vented barrel equipment
- don't use vented barrel equipment for critical appearance applications
- don't change material frequently
- don't use filters in nozzles
- don't use – if possible – a vented barrel machine

## Production

### 4.1 Setting up production

#### 4.1.1 Safety

General recommendations for safety in injection moulding are: appropriate protective clothing should always be worn when handling hot materials and during cleaning operations; continuous and direct removal of processing fumes and dust with a local exhaust system and a re-supply of fresh air will promote good workplace ventilation; avoid eye or skin contact with smoke, fumes, dust and vapours by installing an exhaust hood over the injection moulding machine nozzle. Similar ventilation precautions should be taken for all cleaning operations.

#### 4.1.2 Purging; change-overs

When changing materials during moulding, purging of the cylinder is required. Contamination with foreign or degraded resins can cause problems, such as delamination or black specks. Actual degradation of the to-be moulded material may result in parts which neither look nor perform satisfactorily.

**Start-up** from an empty and clean barrel is straightforward: barrel heaters are set according to the advised temperature profiles, and individual adjustments are made as production starts.

During **breaks in production** the following steps are advised:

1. close off hopper feed
2. empty plasticizing cylinder
3. move screw as far forward as possible
4. reduce barrel temperatures to recommended levels

When starting up again, set the barrel heaters to normal processing temperatures, extrude until residual material is completely purged and begin moulding. The initial shots should be checked for contaminants in the moulded parts.



When a *material change* is necessary, or a *production run ends*, thorough purging of the cylinder is essential to remove all traces of previous polymers. Otherwise results may be unsatisfactory. Problems that may occur include material degradation, resulting in black specks, or, if materials are not compatible, delamination in the moulded parts. In some cases special procedures are necessary.

Purging can be done with nozzles either in place or removed, but removal allows cleaning and inspection for foreign matter. Be sure to avoid danger of splatter when purging. Add purging material with the screw rotating slowly. The purging material should be pressed out immediately and submerged in cold water before being disposed off. Purging should always be done with adequate ventilation.

**Colours and FR**

Extended interruption of production may result in melt discolouration: purging is necessary. Switching colours involves purging until the original colour is completely displaced. When using pigmented or flame-retardant materials, clean the screw and barrel mechanically. During reassembly of threaded components of the injection unit, care must be taken that no grease is in contact with the cylinder, screw surface or nozzle area.

**4.1.3 Purging compounds**

Cycolac resin	ABS, PMMA, SAN
Cycoloy resin	ABS, PMMA, PC, SAN
Lexan resin	PC, PP, PS
Lomod resin	PE, PP, PS
Noryl resin	PS, PMMA
Noryl GTX resin	PE, PP, PMMA
Noryl Xtra resin	Noryl, PS
Supec resin	HDPE, PP, GF PC
Ultem resin	GF PC, PC, PMMA, HDPE
Valox resin	PS, HDPE
Xenoy resin	PS, HDPE

**4.1.4 Details per product**

**FR Cycolac resin**

Production stagnation longer than 10 minutes or with normal shut down: purge with standard ABS.  
When changing to another ABS or another thermoplastic, all FR ABS must be removed before increasing heat settings. Since ABS is not particularly compatible with other polymers, standard ABS is the best purge material. When changing from a high viscosity thermoplastic to FR ABS, decrease temperatures and purge with FR ABS, then make temperature adjustment and continue moulding.

**Cycoloy resin**

Never switch off the heating when PC/ABS is in the barrel: reduce barrel temperatures to 160°C.  
Always purge FR Cycoloy.

**Lexan resin**

As with all PC containing thermoplastics resins, (Cycoloy PC/ABS resin, Xenoy PC/PBT resin), never switch off the heating when the resin is still in the barrel. Reduce to 170°C or clean screw with other material, otherwise black specks will occur or even the screw could be damaged; for transparent parts, it is strongly recommended to clean the screw thoroughly before starting moulding. Ideally a machine should only be used for moulding PC.

**CHANGING FROM OTHER POLYMERS TO LEXAN RESIN**

Thorough purging is especially essential before moulding Lexan resin in transparent, translucent or bright colours. Since the melt temperature required for Lexan resin is often higher than the degradation level of other thermoplastics, it is imperative that all traces of other polymers are purged out before starting moulding Lexan material.  
Extra care must be taken with POM. Its accelerated degradation at even the lowest melt temperatures, as advised for some Lexan grades, will produce unacceptable quantities of formaldehyde.



Contamination with nitrogen-containing polymers such as ABS and PA or FR polymers can cause chemical reactions that may severely degrade the polycarbonate, showing as dark spots in moulded parts. Should this occur after thorough purging of the machine, remove the screw and clean both cylinder and screw. A thorough inspection should be made of cylinder, screw and check rings for cracks and proper fit.

Best purging material is polycarbonate or some proprietary compounds.

#### CHANGING FROM LEXAN RESIN TO OTHER POLYMERS

Where other materials are used after Lexan polymer, thorough purging to remove all traces of Lexan material must be done before the barrel has cooled. Purge with a PMMA and drop the cylinder temperatures if the resins to be moulded afterwards are POM, ABS or PA. Do NOT purge directly with PA or ABS after Lexan resin.

#### INTERRUPTION OF PRODUCTION

Keeping Lexan resin overnight or over a weekend in the cylinder is generally not recommended but can be done in the following way:

- reduce cylinder temperature to 170 to 180°C
- leave heaters on
- ensure that the temperature never drops below 160°C, otherwise Lexan resin will adhere to the cylinder walls and may pull off metal particles and degraded resin as it cools and contracts. This contamination will show as black specks in the mouldings when production is restarted.
- during production delays, empty the screw to prevent overheating.

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#### **Lomod resin**

Lomod resin requires no special purging procedures: normal purging with HDPE, LDPE, PP or PS will do. Because the processing temperatures of these materials are within the same range as used for Lomod resins, there is no need to

reduce cylinder temperatures.

#### **Noryl resin**

PS and PMMA are effective purging materials for all Noryl resins. Purging should be done within the melt temperature range of the particular Noryl grade.

When moulding has to be stopped, the following steps are recommended:

- maintain cylinder temperature for interruptions of up to 15 minutes
- lower cylinder temperature by 40°C for periods from 15 minutes to 2 hours
- reduce further to 170°C for interruptions from 2 to 12 hours
- purge out barrel and shut off heat for periods longer than 12 hours

#### **Noryl Xtra resin**

Purge always with PS after process interruption.

#### **Supec resin**

HDPE, PP or glass-filled PC are suitable materials for purging the barrel after moulding Supec resin.

#### **Ultem resin**

##### CHANGING FROM OTHER POLYMERS TO ULTEM RESIN

Thorough purging is essential when changing to Ultem resins. Since the processing temperature of Ultem resins (350 to 410°C) is well above the degradation level of most other thermoplastics, it is essential to remove all traces of other polymers to avoid contamination resulting in black specks. Best purging material for Ultem resin is glass-filled Lexan reground; drying is not recommended. Purge at the processing temperature of Ultem resin, continue to purge until the actual barrel temperature has reached 350°C, followed by the standard start-up procedure. Chemical purging compounds are not recommended. As with Lexan resin, take extra care with POM even at the lowest temperatures used for moulding Ultem resin. Its accelerated degradation produces unacceptable quantities of formaldehyde. FR polymers which contain nitrogen must be purged completely, otherwise contamination can cause chemical reactions that degrade Ultem resin.

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#### CHANGING FROM ULTEM RESIN TO OTHER POLYMERS

Purging the cylinder after moulding of Ultem resin parts can be done by using Lexan polycarbonate. Put Lexan resin in the hopper when temperature settings are still at the high level as used for Ultem resin. The settings should be reduced to 300°C, however, the moment Lexan material is fed in.

Purging can be completed by high viscosity PE or GE Plastics' Kapronet® purging compound. For stubborn cases purging can be done by using glass fibre-filled Lexan resin.

#### INTERRUPTION OF PRODUCTION

Short breaks: empty barrel and shut off hopper. Stopping production for more than 30 minutes: purge barrel empty and drop temperature settings down to 200°C.

When stopping production for overnight, empty the barrel and drop temperature settings to around 200°C. If stopping for the weekend, switch off temperature settings after purging the barrel.

When shutting down the machine, the hopper must be shut off at the throat and the machine should continue running until all residual resin is run out of the barrel. The screw must be left in its forward-most position with the barrel heaters set at 200°C for long periods of time. This reduces black speck contamination during start-up. If temperatures are dropped too low, Ultem resin will stick on metal parts and pull off particles, that result in black specks. Similar to Lexan resin.

#### **Valox resin**

When changing over to Valox resins from higher melt temperatures or heat sensitive materials, either PS or HDPE may be used as purging material. Due to the 'scrubbing' action of glass fibres, purging for glass-reinforced Valox resin may not be necessary.

#### **Xenoy resin**

Never switch off the heating when PC/PBT is in the barrel: reduce barrel temperatures to 160°C.

#### 4.1.5 Preparation before setting

##### **Part**

- Was the part produced before? On what machine?
- Has the previous experience been recorded?
- How many mouldings are needed? By when?
- Any special measuring equipment needed?
- Weight and size of moulding: cylinder and clamping force?

##### **Material**

- Where is the material stored?
- Is the material pigmented? In what colour?
- Does the material contain recycle? And in what percentage?
- Does the material need pre-drying?
- Temperature and time of pre-drying?
- And with what equipment?

##### **Mould**

- Where is the mould stored? How can it be transported?
- What clamping equipment is needed?
- Does it fit in with the specified machine data, tiebars, core pulling devices, etc.?
- Are the mould and clamping devices ready to use?
- What temperature control is needed and what equipment does this require?

##### **Machine**

- When is the specified machine available?
- Is the machine in good working order, free from problems, lubricated, with clean mould platens etc.?
- What cylinder is needed? And what nozzle?
- Should the cylinder be purged?
- Has the additional equipment been planned: core pulling devices, air ejectors, robots etc.?
- Any trimming equipment, shrink fixtures needed?





#### 4.1.6 Setting mould and machine

##### **Mounting the mould and setting the clamping unit**

- set mould height on the machine with the clamping unit closed
- check clamping devices
- fix mould securely to the lifting tackle, ensuring that the two mould halves remain together, if necessary by bolting
- lock mould and thoroughly tighten up clamping bolts
- set clamping force at desired level
- set mould safety device: low pressure and high pressure
- set mould opening stroke, with damping.
- set ejectors
- set speed of the clamping unit
- set up the mould safety protection
- heat up mould to the required temperature

##### **Setting the injection unit**

- bring injection unit into rear position
- check nozzle radius and diameter
- check penetration depth of nozzle
- check the centring of the nozzle to the sprue bushing
- heat up cylinder
- set cylinder temperatures (not too high) and screw speed
- after having heated up the cylinder, set nozzle contact force
- make sure the mould is closed
- initially set material feed somewhat lower than the required shot weight
- set the position for change-over to hold-on pressure based on safety side
- plasticize stepwise under manual control, while observing how the material feeds: this should be consistent and not in jerky movements
- after a short pause, purge out manually and check the melt temperature
- set injection speed and injection pressure to average values

##### **Setting the machine controls**

- set the operational selector switch to manual
- set injection time, after-pressure time and pause time initially somewhat longer than necessary, then optimize them after a few shots

#### 4.1.7 Starting the injection process

When all settings have been checked, switch over from 'manual' to 'semi-automatic' mode. In general the settings must be optimized after several shots. Take following steps:

- increase or reduce metering
- optimize injection speed
- observe the material cushion in front of the screw
- check pressure build-up during injection
- check cooling time and if possible shorten it
- set screw r.p.m. to a low value: plastification time should be slightly shorter than cooling time
- check mould locking force
- harmonize machine movements to obtain a better balance of speeds, sequence and damping
- if visually acceptable mouldings are being produced, check quality
- where necessary, optimize and store the various functions
- record machine setting data
- ensure that mouldings are correctly taken out and transported away
- ensure quality control
- aim for a 'fully-automatic' machine cycle to ensure uniform moulding quality

#### 4.1.8 Setting temperatures, speeds and pressures

##### **Temperatures**

Cylinder-, mould- and melt temperature settings as advised are guidelines, to be used for starting up the production. They are typical for most applications. However, where part geometry and mould design demand for it, higher melt temperatures can be used: the residence times at those temperatures should be kept as short as possible. Too high melt temperatures may result in colour changes when pigmented resins are used.

##### **Injection speed**

Injection speed is largely governed by the complexity of the part, the mould quality and the gating system. Slow injection speeds should be used during start-up.

However, fast injection speeds in general are desirable;

they - avoid premature freezing of the melt

- reduce visibility of weld lines
- give better welding of weld lines
- increase surface gloss
- keep melt temperature in the mould at a higher level
- improve transfer of pressure in the mould
- reduce overall orientation

Several effects can be created by changing the screw advance speed during injection.

A slower speed at the **start** of injection

- reduces mould deformation
- reduces tendency for jetting
- reduces matt spots in the gate area

A slower speed at the **end** of injection

- can reduce variation of properties of the moulding
- enables reduction of clamping force
- improves venting due to reduction of air compression

Profiled injection speed can control shear in some areas of the moulding, e.g. through grille areas etc.

### **Injection pressure**

The injection pressure should be established to mould full parts consistently with a satisfactory finish – free of sink marks, weld lines or similar defects. The level of injection pressure, which should always be started at the minimum level, depends on many things:

- type and grade of material
- complexity of the part
- quality and polish of the mould
- type of gating
- material viscosity

Generally, the lowest pressures which still provide the desired properties, appearance and moulding cycle are preferred.

### **After pressure (hold pressure)**

After pressure compensates for volume shrinkage of the melt during cooling in the mould. It should be maintained until the 'gate is frozen': the corresponding duration of after pressure should result in a constant part weight during moulding.

Insufficient holding pressure may lead to:

- sink marks
- voids
- variations in part dimensions
- increased shrinkage

Too high holding pressure may lead to:

- problems with ejection of the moulding
- stress in the gate area
- warpage

A decrease of the holding pressure at the end of the holding pressure time :

- reduces internal stresses
- reduces warpage because differences in shrinkage in the moulding far and close to the gate are reduced

Since after pressure is mould-related, depending on surface quality, part thickness, shape of gating, etc, it is difficult to recommend exact levels of after pressure.

For GE Plastics' resins, after pressure may vary from 30 to 80% of the injection pressure.

### **Back pressure**

Back Pressure has two functions:

1. it consolidates the melt by excluding air, thereby ensuring consistency of shot volume and removing splay caused by entrapped air.
2. it increases shear on the material: high shear may be necessary for masterbatching, dry colouring, mixing additives and sometimes to obtain a homogeneous melt with low-compression screws.

High back pressure is also used in structural foam moulding to prevent pre-blowing of the blowing agent. It can be used in a similar way for solid mouldings as a trick to reduce splay caused by (too high) moisture content.



The main function of back pressure is to improve mixing of the material: in most cases a low back pressure of 4 to 5 bar is sufficient to get a homogeneous melt without overheating the material. The maximum level of back pressure is related to screw diameter and screw r.p.m. Attention must be paid when moulding flame retardant, glass fibre-filled, pigmented resins and polymer blends. In general, levels of back pressure should not exceed 10 bar.

#### 4.1.9 Mould temperature control

##### **needs to**

- heat up the mould to operating temperature - before production
- remove heat from mould cavity and control tool temperature - during production
- keep mould at uniform temperature - during production

##### **results in**

- optimization of cycle time
- insurance of high and uniform quality of mouldings

##### **Mould temperature**

- very important parameter
- controls cycle time
- controls product properties

*surface appearance*

*dimensions*

*shrinkage*

*warpage*

*crystallization rate*

*moulded-in stress levels*

*thermal behaviour of the moulded parts*

- Amorphous materials

##### **hot moulds**

- improve properties
- no dramatic change of shrinkage values

##### **cold moulds**

- filling difficulties
- high injection pressures needed
- high melt temperature needed

- Semi-crystalline materials

##### **hot moulds**

- higher level of in-mould crystallization
- high shrinkage values

##### **cold moulds**

- crystallization after moulding
- danger of warpage during use of part

##### **Water-based or oil-based units**

- mould temperature below 100°C: water-based
- mould temperature above 100°C: oil-based or pressurized water-based
- heat transmission of oil is about half that of water: heat transmission surface area with oil is twice as big as for water
- pipes and couplings must take the heat requirements

##### **Mould cooling system**

- periodically clean entire temperature control circuit by flushing with a special solution: removes dirt and lime
- use insulating plates to insulate mould from machine
  - reduces the time to heat the mould up to the required temperature
  - extremely important when using hot-manifold and hot-runner moulds



## 4.2 Optimizing production

### 4.2.1 How to improve venting

Whenever a given mould creates problems with venting, such as burn marks or short shots, the first thing to do is to lower the injection speed. This does not increase venting, but it lowers the amount of air that has to leave the mould within a certain period of time. No burn marks on the part due to the diesel effect: as air cannot escape quickly enough, it will be compressed, its heat content will be concentrated in a small volume, resulting in a large temperature increase causing the incoming plastic to burn, (pressure x volume = constant). However, it could be necessary to increase the injection pressure in order to fill the part.

If lowering the injection speed does not help, the venting should be increased. The amount of venting that is possible or required can be tested by taping very thin copper foil on the closing surfaces of the mould. Starting with 0.01 mm thick foil and gradually going thicker, it can be found by trial and error how much the venting can be increased before the part will show flash. Attention when soft moulds are used: the copper foil may damage the mould surface.

### 4.2.2 How to improve mould release

Apart using well-known silicones-free release agents – not to be used when mouldings are painted or decorated afterwards – changing processing conditions can influence mould release. With beaker-shaped mouldings, it is important to keep the core lower in temperature than the cavity the part will shrink on the core and not stick in the cavity, where no ejector pins are available. This requires cooling the mould with separate fluid circuits. In general it is important to closely control the mould temperature. The temperature should not fluctuate too much, or increase in an uncontrolled way.

A well-designed cooling layout, together with a correct way of connecting the various cooling channels – a 'parallel' layout rather than a 'serial' one – can help to keep the mould temperature as even as possible over the total mould surface.

Overpacking – too high injection pressure, for too long – can create release problems: lowering injection pressure obviously is needed.

Too high mould temperature can lead to part warpage; too low mould temperature can result in insufficient flow, leading to overpacking. Increase of cooling time often has a positive effect.

Although mould release is different for each GE Plastics' resin, mostly high injection pressures and overfilling are the major causes of problems. A good way of checking is weight control of the parts during production.

### 4.2.3 How to influence mould shrinkage

Factors that influence shrinkage are cavity pressure and aftershrinkage. Cavity pressure is dependent upon mould temperature, melt temperature, injection speed, injection pressure, level of afterpressure and afterpressure time and, most importantly, the dimensions of gate- and runner systems (loss of pressure). Main parameters are injection pressure, afterpressure and afterpressure time. Parameters like back pressure, melt- and mould temperature have less influence on mould shrinkage.

Aftershrinkage depends on the temperature of the part when it leaves the mould. This temperature again relates to the melt temperature, mould temperature and cooling time.

Parts moulded out of materials such as Noryl GTX resin can show increased dimensions resulting from pick-up of moisture in the air, due to the hygroscopic behaviour of the polyamide present in Noryl GTX resin. The level of this moisture pick-up and the speed with which it occurs depend on relative humidity, (RH), temperature and wall thickness of the moulding. At 23°C and 50% RH saturation can take months.

### 4.2.4 How to use hot runner tooling systems

Hot runners tend to make the whole process of moulding in general more susceptible to material degradation; not only due to longer residence times at higher temperatures, but also through the often not completely balanced flow/temperature control in a hot runner system. This may result in big differences in temperature in the various zones of hot runner blocks or nozzles.



## Quality assurance

### 5.1 Quality control

Effective quality control enables simple yet accurate testing of materials and parts for behaviour and defects under processing conditions. Accepting the quality of the material, the main points are material degradation and unsatisfactory part performance.

Where materials have a narrow processing window, deviations in mechanical, thermal and physical properties can occur. The narrower this window, the harder it becomes to maintain part consistency, and thus rejection rates increase. Material that can be processed using a wide range of processing conditions provide an almost negligible rejection rate. This processing flexibility, however, makes the discovery of deviations from the optimum on moulded parts more difficult. Successful quality control is based on the comparison of production parts with samples of a good quality and known properties.

Quality control systems based on statistical process models, such as SPC, are recommended.

For all parts, however, control methods should be related to the desired performance of the application, and, not least, the cost of it. The effects of costly engineering to attain certain unnecessarily high standards should always be borne in mind.

### 5.2 Visual control

This is the most important control method, as there is mostly a direct correlation between appearance and properties of the moulding. Extensive descriptions of deviations are discussed in Chapter 6 'Part Defects and Corrective Actions'.

### 5.3 Mechanical control

Due to the varying shapes and sizes of moulded parts, mechanical testing can be difficult. It is therefore advisable to prescribe procedure, conditions and equipment carefully, and to experiment with testing. Mechanical testing demonstrate whether material quality and processing conditions affect th

Also very important is the lowering of the temperature of the hot runner when the moulding process is interrupted, (in case of problems for example), otherwise too much degradation of the material might occur. Purging the cylinder is rather easy, whilst purging the hot runner system is much more difficult. Sometimes however it may be necessary, otherwise the mould would be filled with degraded material. This might be difficult to remove from the mould surface and it could lead to staining. Also very important with hot runner systems is the option of an electrical circuit that allows gradual heating up. Eventual moisture present in the heater cartridges can evaporate: it avoids the chance of short circuiting. This is especially important in case a hot runner system has not been used for a long period of time. Also important is the possibility to heat the zones separately by using different control units. The power can be varied and thus uniform temperatures created.

#### 4.2.5 How to save energy

Tips that not only save money, but also material:

- do not keep the machine nozzle always against the mould: after the gate is frozen, pull the cylinder back from the mould directly after plasticizing – in case of a shut-off nozzle
- use insulated plates between mould and machine
- aim for optimal control of the mould temperature; the allowed temperature difference between 'temp-in' and 'temp-out' of the coolant is a balance between quality of moulding (1 to 2°C) and economics (3 to 5°C)
- keep screw r.p.m. at a low level: the plastification time should be slightly shorter than the cooling time
- do not use a cylinder with a too high capacity for the actual shot weight



mechanical properties of the part, and can also be related to practical requirements. A common procedure is the falling dart test, which assesses the component's ductility. The prime objective is to check for material degradation during processing. This affects impact properties, as do other deviations from optimal processing such as bubbles, sink marks, weak knitlines, etc.

#### 5.4 Weight control

An economical, fast and easy method that can be carried out at the production location. Often preferred over dimensional methods, since weight variations will be more readily noticeable than those of dimensions. It can also assist in checking bubbles and voids, or other deviations from the filling rate of the cavity in the tool. Wide variations in weights of parts can indicate insufficient production and/or machine tolerances. Stabilizing part weight in general indicates stabilized processing conditions.

#### 5.5 Dimensional stability

Factors such as orientation of polymer chains, internal stresses and filling rate of the cavity have an influence on performance characteristics of a part. Dimensional stability is thus dependent upon the control of all setting parameters on the moulding machine. Thermal stability tests can be carried out for shrinkage and/or deformation of parts following pre-conditioning at just above the resin's heat distortion temperature.

Complete mouldings should be used and a detailed study of each application is required to set correct parameters, using mouldings produced under optimal conditions.

#### 5.6 Stress control

Due to tool or part design it is not always possible to produce really stress-free parts. For transparent materials such as Lexan resin it is often advisable to produce pre-production test

mouldings: a light source with a linear polarized filter can then be used to detect internal stress concentrations. Stress levels can also be checked using stress corrosive fluids such as TnBP for Noryl resin and toluol N propanol for Lexan resin. (GE Plastics' representatives can supply more information.)

A simple but effective way to check stress in parts moulded out of Lexan resin is to observe them after 24 hours immersion in a 80°C solution of 100 g dishwashing powder with 10 g gloss agent in 1 liter water.

#### 5.7 Viscosity control

Measuring viscosity of plastics materials can be used to check possible degradation of the resin resulting from injection moulding, UV ageing/weathering or heat ageing. Differences in flow 'before and after' indicate material degradation: any deviation from original granulate flow could be related to either 'abusive' moulding or non-controlled part ageing.

For Lexan PC and PC blends such as Cycoloy and Xenoy resins, the intrinsic viscosity or IV method is used.

It demonstrates whether the material has been properly pre-dried and/or degraded during moulding. The percentage loss in IV of the material due to moulding of the part is an indication of material degradation. Information on exact figures can be obtained via GE Plastics' representatives. For all materials the MVR (melt volume rate) or MFR (melt flow rate) can be used – same test, just a different way of measuring the result: MVR in cm<sup>3</sup>/10 min., MFR in g/10 min. The delta flow data of MVR and MFR show the change of the material during and after processing. During processing, phenomena such as thermal degradation, crosslinking and other desired or undesired processes can occur. These are very dependent upon moulding conditions, part design and tool design.



## 5.8 Other methods

Very reliable methods of quality control are tests according to government and agency standards such as VDE, KEMA, SEMKO, NEMKO, etc. For these standards, test methods for both application and material are provided. This avoids possible confusion between moulder and end-user. More and more computer-based control systems are used nowadays. Many new software and hardware tools enhances the quality of moulds, machines and mouldings produced with them. They give possibilities to optimize, visualize and monitor basic settings of the injection moulding machine. Using pressure sensors in moulds, filling phases can be analyzed to get information about orientation, appearance and crystallinity of moulded parts. Deviations of several shots following each other can be calculated statistically and monitored afterwards. Differences in quality can be signalled immediately.

# 6

## Part defects and corrective actions

### 6.1 Fault diagnosis

If a part has been produced satisfactorily and it goes wrong, something has changed. The principle is not to change conditions immediately. The **cause** should be *identified* and *rectified*.

Never adjust one condition to compensate for a failure or change in another condition. For example, if melt temperature has increased, *don't* reduce speeds or pressures or mould temperature to compensate. *Identify problem*, that is to say reduce melt temperature to what it was before, by checking and replacing thermocouples, etc.

#### Ask questions

- what has *changed*?
- what is fault?
- when did it start?
- how often does it occur?
- where is fault?
- is the fault randomly situated or always in same place?
- etc.

#### Identify causes of defects

- test, observe, conclude and study 'history of faults'
- injection speed: test
- screw speed: test
- back pressure: test
- melt temperature: test
- etc.
- machine: check
  - heating of cylinder*
  - mould temperature control*
  - material cushion*
  - locking of mould*
  - etc.*





## 6.2 Fault descriptions, causes and actions

### 6.2.1 Black specks

Dark spots  
due to thermal  
damage



#### DESCRIPTION

Small black areas (spots) inside the material, mostly present in transparent resins.

#### CAUSES

##### *machine*

- down time too long
- barrel switched off over a long period of time
- poor purging of barrel
- dirty plasticizing unit
- inadequate nozzle

##### *mould*

- dead edges in gate/runner system
- ##### *material*
- granule impurities
  - degradation by other resins
  - pick-up of degraded material from cylinder wall during cooling

#### ACTIONS — IN ORDER AS SHOWN

1. purge with an appropriate material  
in general: Kapronet  
for Lexan PC: ground acrylic or regrind Lexan resin  
for Ultem resin: regrind Ultem resin or glass-filled Lexan resin – don't drop temp. settings while purging;  
(for details on purging, see pages 19 to 24)
2. check for impurities: use uncontaminated material, do proper housekeeping
3. check and adjust melt temperature
- check for dead edges: nozzle, back flow valve, gates/runners
- check for screw wear

### 6.2.2 Blisters, bubbles

Blisters can  
cause bulges on  
the surface



#### DESCRIPTION

Small air-or gas-filled hollows in the moulding, cooling voids.

#### CAUSES

##### *machine*

- injection pressure too low
- inadequate functioning of back flow valve
- suck-back too long
- plasticizing too fast
- air trap in the hopper feed
- improper feed

##### *mould*

- volatiles and trapped gas
- mould temperature too low
- thin to thick transition

##### *material*

- melt overheating

#### ACTIONS — IN ORDER AS SHOWN

1. control holding / injection pressure
2. increase back pressure
3. increase mould temperature
4. check back flow valve
5. allow for adequate venting
6. enlarge gate
7. shorten land length





### 6.2.3 Blush / flow marks

Dull spot  
(corona) near  
the sprue



#### DESCRIPTION

Blush and flow marks are the result of variations in material temperature, caused by the temperature gradient between machine nozzle and mould sprue bushing. A halo around the direct sprue is the result of cold material in the nozzle tip section. Eliminating the temperature gradient will minimize the blush and halo effects.

#### CAUSES

- |  |                             |
|--|-----------------------------|
| <i>machine</i>                         | <i>mould</i>                |
| • injection speed too slow or too fast | • inadequate mould cooling  |
| • injection pressure too low           | • mould too hot around gate |
| • hold pressure too long               | • mould too cold            |
|  | • gate too small            |
|  | • wrong gate location       |
|  | • gate land length too long |
|  | • wrong hot runner system   |
|  | <i>material</i>             |
|  | • melt temperature too low  |

#### ACTIONS — IN ORDER AS SHOWN

1. adapt injection speed
2. add a large cold slug area
3. add cold wells at the end of runner systems
4. control nozzle heat better: if necessary add beryllium copper tip (not recommended for FR resins)
5. shorten or eliminate standard sprue bushing:
- use a hot sprue bushing
- clean flow must exist from the cylinder, adaptor, nozzle and tip: avoid and eliminate any dead pockets or sections

### marks / diesel effect

Diesel effect  
(burns) due to  
entrapped air at  
the end of the  
flow path



#### DESCRIPTION

Burn marks are (often) brown streaks. They are usually caused by overheating the material due to entrapped air (diesel effect): this causes the darkening in colour.

#### CAUSES

- |                                 |  |
|---------------------------------|--|
| <i>machine</i>                  | <i>mould</i>                                 |
| • problems with back flow valve | • inadequate venting: entrapped air          |
| • injection speed too fast      | • frictional burning                         |
| • back pressure too high        | • check sprue diameter                       |
|                                 | <i>material</i>                              |
|                                 | • melt too hot or too cold: may create shear |

#### ACTIONS — IN ORDER AS SHOWN

1. check venting channels for dirt
2. decrease injection speed
3. decrease injection pressure
4. use programmed injection
5. check for heater malfunctioning
6. reduce screw r.p.m.
7. decrease nozzle temperature
8. reduce melt temperature
9. improve mould cavity venting
  - add vents to ejector pins
  - add vents to parting line of part
10. enlarge gate to reduce frictional burning
11. alter position and/or increase gate size

### 6.2.5 Delamination

Cosmetics  
article  
with flaked off  
'skin'



#### DESCRIPTION

Separation of layers in the moulded part that can be peeled off: flaking of surface layers. It results from insufficient layer bonding due to inhomogeneities and high shear stresses.

#### CAUSES

##### *machine*

- injection speed too high

##### *mould*

- mould too cold
- sharp corners in gate area
- shear heat caused at sharp corners

##### *material*

- melt too hot
- poorly melted
- incompatible colour dyes
- cross contamination with other polymers
- too much use of recycled material

#### ACTIONS — IN ORDER AS SHOWN

1. increase melt temperature
2. increase mould temperature
3. decrease injection speed
4. eliminate contamination
5. check percentage regrind
6. dry material
7. purge equipment
8. change material
9. radius all sharp corners at gate

#### Actions of part

#### DESCRIPTION

Excessive shrinkage means part dimensions differing from expected ones; amorphous resins behave differently to semi-crystalline materials.

#### CAUSES

##### *machine*

- injection pressure too low
- injection hold pressure time too short
- overall cycle too short
- back flow valve cracked
- excessive cylinder clearance
- heater bands burned out

##### *mould*

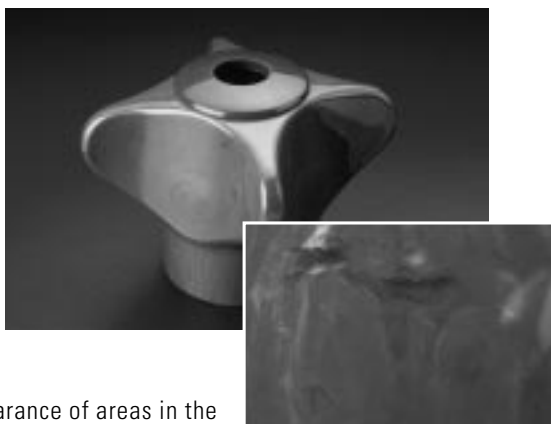
- too hot
- gates too small (related to inadequate pressures)
- gating in the wrong place
- mould too small

#### ACTIONS — IN ORDER AS SHOWN

1. increase injection pressure
2. increase cooling time
3. increase mould temperature
4. maintain uniform cycle time operation
5. check machine for erratic operation
6. check the percentage regrind to virgin material
7. increase gate size
8. reduce gate land length
9. relocate gate if glass-filled compounds
10. balance runner and/or gate system
11. reduce number of cavities to balanced system

### 6.2.7 Discolouration

Colour streaks  
due to poor  
blending in the  
plasticizing  
unit



#### DESCRIPTION

The appearance of areas in the moulding with a deviating colour.

#### CAUSES

##### *machine*

- contamination

##### *mould*

- check sprue diameter
- pin-point too small
- poor venting

##### *material*

- melt too hot or too low: may create shear
- long residence time
- instability of polymer/pigments

#### ACTIONS — IN ORDER AS SHOWN

1. purge heating cylinder
2. lower material temperature by
  - reducing cylinder temperature
  - decreasing screw speed
  - reducing back pressure
3. lower nozzle temperature
4. check residence time
5. check machinery purging
6. shorten overall cycle
7. check hopper and feed zone for contaminants
8. check for proper cooling of ram and feed zone
9. provide additional vents in mould
10. move mould to smaller shot size press to reduce residence time

Large area  
overspraying



#### DESCRIPTION

A film of material attached to the moulding at the mould parting line.

#### CAUSES

##### *machine*

- clamping pressure too low
- injection pressure too high
- injection speed too fast

##### *mould*

- inadequate mould supports
- clamping force too low
- damaged mould surface: parting line
- excessive projected area

##### *material*

- melt too hot
- viscosity too low

#### ACTIONS — IN ORDER AS SHOWN

1. reduce injection speed
2. reduce injection pressure and/or booster time
3. increase clamping force
4. check mould for proper mould support and/or parallelism
5. reduce melt temperature
6. reduce mould temperature
7. check excessive vent depths
8. change to higher clamping machine



### 6.2.9 Jetting

Jetting starting at the gate, spreading over the entire moulded part



#### DESCRIPTION

A turbulent flow in the resin melt: the melt strand enters the cavity in an uncontrolled way. Due to cooling down, the strand is not fused homogeneously with the melt that follows. It shows as a serpentine line on the part surface. Too little restriction when filling the cavity: material is injected in empty space (wrong gate angle).

#### CAUSES

##### *machine*

- injection speed too fast

##### *mould*

- mould too cold
- gates too small
- gate land length wrong
- wrong gate location

##### *material*

- melt too cold

#### ACTIONS — IN ORDER AS SHOWN

1. decrease injection speed
  2. check nozzle heating
  3. increase mould temperature
  4. increase melt temperature
  5. increase gate size
  6. avoid gating at thick section
  7. modify gate location or angle: directly into wall or pin
- use tab gate or submarine plus pin

#### DESCRIPTION

Pitting is the presence of unmelted particles due to difficult dispersion of additives, wrong mixing or cross-linking during processing.

#### CAUSES

##### *machine*

- wrong or worn out screw, giving hang-ups
- melt temperature too low
- injection pressure too low

##### *mould*

- shear in gating
- sharp corners

##### *material*

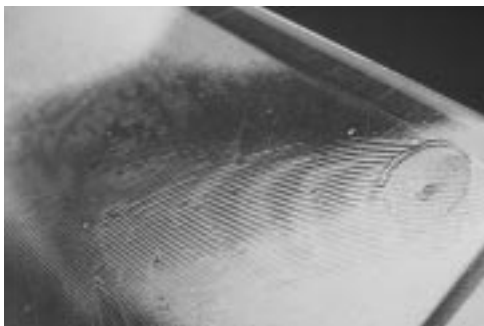
- inhomogeneous material
- contamination

#### ACTIONS — IN ORDER AS SHOWN

1. get shear down
2. lower back pressure
3. decrease injection speed
4. change temperature profile
5. check regrind percentage
6. check shot size vs part
7. check hot-runner: torpedoes

### 6.2.11 Record grooves

Concentric  
record  
grooves



#### DESCRIPTION

Resembles the grooves of gramophone records. At slow speed - as material nears cold tool - it loses its flow (below HDT) before actual contact. The melt that follows flows over cooled melt, to repeat the cycle.

#### CAUSES

##### *machine*

- injection speed too low
- injection pressure too low

##### *mould*

- mould too cold
- different texture of mould halves:  
polished vs coarse grain

##### *material*

- melt too cold

#### ACTIONS — IN ORDER AS SHOWN

1. increase injection speed
2. increase injection pressure
3. increase melt temperature
4. increase mould temperature
5. check mould textures

### se problems

#### 6.2.12.1 *Sticking in cavity*

#### DESCRIPTION

At end of cycle, the moulding does not release from the mould but sticks in the cavity (female mould side).

#### CAUSES

##### *machine*

- injection pressure too high
- injection speed too high
- holding time too long
- too much material feed

##### *mould*

- cavity too hot – release is better from hot mould  
(20°C below HDT)
- mould too cold
- poor mould finish

##### *material*

- melt too hot

#### ACTIONS — IN ORDER AS SHOWN

1. check cycle time: cooling
2. decrease injection pressure
3. decrease injection hold time
4. decrease injection speed
5. decrease booster time
6. reduce and adjust feed for constant cushion
7. check for poor mould finish or corrosion on  
mould surface
8. increase mould opening time
9. decrease material temperature by lowering cylinder  
temperatures and/or nozzle
10. lower mould temperature
11. adjust the cavity temperature to a 20°C differential  
between mould halves
12. check mould for undercuts and/or insufficient  
draft and taper
13. use proper mould release

6.2.12.2 **Sticking on core****DESCRIPTION**

At end of cycle, the moulding does not release from the mould but sticks on the core (male mould side).

**CAUSES***machine*

- injection pressure too high

*mould*

- core too hot
- core bending
- creation of vacuum — especially on thin-walled parts

**ACTIONS — IN ORDER AS SHOWN**

1. check cycle time: cooling
2. decrease injection pressure
3. decrease injection hold time
4. decrease booster time
5. adjust feed for constant cushion
6. decrease mould-closed time
7. increase core temperature
8. decrease cylinder and nozzle temperature
9. check mould for undercuts and/or insufficient draft
10. check mould for bending: rule of thumb is 1:5 for core diameter to core length

**ng of sprue****DESCRIPTION**

At end of cycle, the sprue does not release from the mould but sticks in the sprue bushing.

**CAUSES***machine*

- injection pressure too high
- too much material feed
- nozzle frozen
- nozzle diameter too large for sprue bush
- inadequate draft angle
- drool from nozzle

*mould*

- too hot
- ineffective sprue pullers

**ACTIONS — IN ORDER AS SHOWN**

1. decrease injection pressure
2. decrease injection hold time
3. decrease booster time
4. increase die-closed time
5. decrease mould temperature at sprue bushing
6. leave nozzle against mould: no pull back
7. raise nozzle temperature
8. check incorrect seat between nozzle and sprue: sizes and alignment of holes in nozzle and sprue bushing
9. sprue bushing hole must be larger: reduce nozzle diameter for sprue bushing being used
10. check polishing of sprue
11. check proper design of sprue puller pin
12. check cone of sprue: usually 1:20, for difficult jobs 1:15
13. provide more effective sprue puller:
  - increase sprue puller by increasing taper of sprue puller
  - polish worn or rough sprue bushing



### 6.2.13 Short shots

Solidified flow  
front on a  
glass fibre  
reinforced  
housing



#### DESCRIPTION

Resulting from incomplete filling of the mould: parts of the moulding are not formed.

#### CAUSES

##### *machine*

- improper feed
- injection pressure too low
- injection speed too low
- injection time too short
- faulty back flow valve ring

##### *mould*

- poor mould venting
- mould too cold

##### *material*

- melt temperature too low
- viscosity too high

#### ACTIONS — IN ORDER AS SHOWN

1. increase dosage
2. increase injection pressure
3. increase booster time forward
4. increase material temperature by increasing cylinder temperatures
5. increase mould temperature, if glass-filled
6. check material flow length vs wall section thickness
7. increase nozzle diameter
8. check restrictions of nozzle, runners and actual gating
9. increase gate size of sprue and runner system



## 6.2.14 Sink marks

Sink marks  
due to wall  
thickness  
variations



### DESCRIPTION

Visible defects resulting from insufficient cooling before removal from the mould. A heavy rib intersecting a thin wall may show up sink marks: these are very difficult to eliminate by varying processing conditions. Too high holding pressure – useless when gating is too small – creates very high stresses in gate areas.

### CAUSES

#### *machine*

- injection pressure too low
- injection pressure time too short
- short of shot capacity

#### *mould*

- mould temperature too high: too high shrinkage
- gate too small: leads to early cooling/freezing at the gate, holding pressure cannot help anymore to compensate for the shrinkage
- land length too long
- wrong dimensions rib vs wall

#### *material*

- melt too hot

### ACTIONS — IN ORDER AS SHOWN

1. increase injection speed to maximum range
2. sometimes lower injection speed: crystalline materials
3. increase injection hold time
4. increase injection pressure
5. reduce melt temperature
6. reduce mould temperature
7. check for hot spots: separate water channels in cooling system / add heat pipes such as thermal pins or beryllium copper slugs for spot cooling
8. enlarge and/or add vents to mould parting line
9. increase size of sprue and/or runners
10. increase gate size and reduce gate land length
11. relocate gate next to heavy or thicker areas
12. core out heavy wall sections where possible
13. incorporate textured surfaces





6.2.15 **Splay / streaks**6.2.15.1 **Splay****DESCRIPTION**

Splay marks, silver streaks, splash marks are the result of

- (a) moisture on the pellets which should be removed under recommended drying times and temperatures
- (b) products of degradation due to overheating
- (c) residual non-aqueous volatiles in material
- (a) and (c) will produce fine lines emanating from the gate all over the part whereas (b) will show up as coarse lines, lumps in sections of the moulded parts.

**CAUSES***machine*

- degraded material

*hot spot in cylinder**material hang-up area at nozzle tips or adaptors*

- injection pressure too low or too high
- injection speed too low or too high
- back pressure too low

*mould*

- frictional burning at gate, in machine nozzle or hot runner
- trapped volatiles

*material*

- melt too hot
- contamination in resin
- excessive moisture
- Noryl resin: degradation of material due to too long pre-drying at high temperatures

**ACTIONS — IN ORDER AS SHOWN**

1. check pre-drying: dry material before use
2. check moisture content after pre-drying
3. check effectiveness of drying equipment: temperature and time
4. lower nozzle temperature
5. lower material temperature by:
  - lowering cylinder temperature
  - decreasing screw speed
  - lowering back pressure

6. decrease injection speed
7. raise mould temperature
8. shorten or eliminate screw decompression
9. shorten overall cycle
10. increase back pressure; in case of drooling, reduce back pressure
11. check for drooling
12. check for contamination (e.g. water or oil leaking into mould cavity)
13. barrel purging (hang-ups)
14. allow for adequate venting
15. open gates
16. move mould to smaller shot-size press

6.2.15.2 **Gate splay****DESCRIPTION**

Gate splay is the appearance of dull spots around the gate, resulting from temperature differences in the material, (too high shear forces tearing the surface layer). Often moisture streaking resulting from improper pre-drying.

**CAUSES***machine*

- injection too fast

*mould*

- mould too cold
- gate too small
- improper gate location or too sharp angle gate to part

*material*

- melt too cold

**ACTIONS — IN ORDER AS SHOWN**

1. decrease injection speed
2. increase mould temperature
3. increase melt temperature
4. increase gate size
5. change gate location



### 6.2.15.3 **Streaking**

#### DESCRIPTION

The appearance of large, dull and lamellar areas on the surface of a moulding.

#### CAUSES

##### *machine*

- damaged back flow valve ring

##### *mould*

- areas of hang-up
- hot spots

##### *material*

- contamination caused by stock or machine

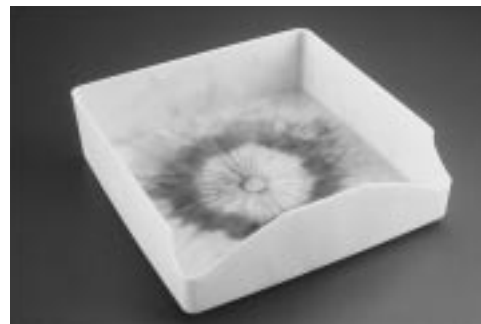
*if steady pattern: machine*

*if erratic pattern: material pigmentation /*

*instability of material*

#### ACTIONS — IN ORDER AS SHOWN

1. check for material contamination by other resins
2. check barrel purging
3. check for cracked or worn back flow valve ring
4. check for worn feed screw
5. check for excessive clearance on screw/barrel dimensions
6. check for overheated cylinder heater bands
7. check for overheated nozzle heater bands



Burnt streaks due to excessive residence time in the plasticizing cylinder



Streaks due to excessive moisture content of the granules



Air streak (near the sprue) due to sucked in air during decompression



Glass fibre streaks (clearly visible weld line)

6.2.16 **Stringing****DESCRIPTION**

Stringing is the appearance of a thin plastic string coming from the sprue.

**CAUSES***machine*

- back pressure too high
- nozzle temperature too high

*mould*

- wrong sprue

*material*

- insufficient melt strength

**CORRECTIONS — TRY IN ORDER AS SHOWN**

1. use suck back: only for crystalline materials
2. lower back pressure
3. lower or increase nozzle temperature
4. use different temperature profile
5. do not use sprue breaks

**DESCRIPTION**

Vacuole hollows ('empty bubbles') in the moulding, due to thermal shrinkage that draws material away from the fluid core of a part.

**CAUSES***machine*

- injection pressure too low
- injection pressure time too short
- injection speed too high
- back pressure too low

*mould*

- mould temperature too low
- incorrect material flow
- part wall too thick

*material*

- melt too hot
- wrong material grade: some Lexan resin types more sensitive

**ACTIONS — IN ORDER AS SHOWN**

1. decrease injection speed to medium range
2. increase holding time
3. reduce melt temperature
4. increase mould temperature
5. check gate size: too small results in freezing at gate with voids and sinks in other areas of the part
6. increase gate size and reduce gate land length
7. increase nozzle size and/or runner system
8. redesign part to obtain equal wall sections



6.2.18 **Warpage, part distortion**

DESCRIPTION

A dimensional deformation of the moulding resulting from frozen-in stress, or because the part was taken too hot from the mould. Basically it is due to pressure differences between areas.

CAUSES

*part*

- wrong part design
- part too heavy

*machine*

- insufficient cooling time
- too high injection pressure

*mould*

- wrong gate location: different shrinkage in different flow directions

- too big undercuts
- inadequate ejector pins
- cavity too hot

*material*

- orientation of fillers
- wrong material choice

ACTIONS — IN ORDER AS SHOWN

1. equalize temperature of both mould halves
  2. observe mould for uniform part ejection
  3. check handling of parts after ejection from mould
  4. check part weight: take care with Valox resin
  5. increase injection hold time
  6. increase cooling time
  7. increase or reduce injection pressure
  8. increase mould close time
  9. increase or reduce mould temperature
  10. set differential mould temperatures to counteract warpage due to part geometry
  11. use shrink fixtures and jigs for uniform cooling of the part
  12. check gate locations and total number of gates to reduce orientation
  13. additional gates may be required to overcome overpacking or underpacking on large parts
  14. increase gate dimensions
  15. change gate location if glass-filled, notice fibre orientation
- redesign part to equalize wall variation in moulded part – heavy and thin walls in same part create differential shrinkage stresses

Weld lines / knit lines

Colour differences at a weld line



DESCRIPTION

These lines occur where two plastics flow fronts in the mould meet. The streams of plastic should be hot enough to fuse adequately. Weld lines are not just surface marks, but can be points of weakness: notches, stress raisers.

CAUSES

*part*

- wrong part design

*machine*

- injection speed too slow
- injection pressure too low
- injection time forward too short

*mould*

- mould too cold
- insufficient venting
- inaccurate functioning of back flow valve
- distance from gate excessive

*material*

- melt too cold

ACTIONS — IN ORDER AS SHOWN

1. increase injection pressure
2. increase injection hold time
3. increase injection speed
4. raise melt temperature by increasing cylinder temperatures
5. raise mould temperature
6. check for proper venting of the part
7. vent the cavity in the weld area
8. provide an overflow well next to the weld area
9. change gate location to alter flow pattern

>>>

10. increase gate and/or main runner system
11. reduce gate land length
12. spot heat particular area with thermal pins or cartridge heaters
13. use textured surfaces

## 7

## Reusing materials

Thermoplastics resins in general can be recycled into similar applications: this means that a company can grind, clean and eventually upgrade the material. GE Plastics' product range of selected post-consumer recycle materials is called Remex™ Engineering Plastics. This activity of reusing materials is called '*recycling*'.

During production, such as with injection moulding, sprues, faulty mouldings, short shots, and so on, can be reground directly in the production facility and reused. This can be done by using reground resin on its own, or by mixing regrind with virgin material. This activity of reusing materials is called '*regrinding*'. To avoid misunderstanding, only '*regrinding*' will be discussed here.

Sprues, runners and faulty mouldings produced from GE Plastics' resins can all be reground. Care should be taken to ensure that reground material is not degraded and is clean and free from impurities. Parts that show traces of over heating or burning, and also parts with humidity related defects such as splash, should never be reground. Obviously reground materials should be of the same composition and not be mixed with other plastic grades.

If there is the slightest doubt whether degradation or contamination has occurred, the material should not be reused. It is also very important that reground materials are properly pre-dried, as with virgin materials.

Although many resins show minimal reduction in properties after regrinding, special attention is required to ensure that reground materials in principle are not used for impact critical applications. Care must also be taken when reusing flame retardant or heavily pigmented materials.



In general, it is very difficult to quantify what mixing percentages of reground: virgin material are possible. These differ from case to case, being related to customer-defined part quality requirements and applicable standards and regulations.

The following factors should be borne in mind when using reground materials:

- moulding conditions of first moulding process
- impact behaviour of final parts
- flame retardancy, UL requirements
- UV resistance
- colour stability
- chemical resistance
- physical properties
- preparation of material prior to use
- disposal of dirty parts
- proper pre-drying
- moulding conditions of second moulding process

GE Plastics understands that the plastics processing community wants to take advantage of this important feature of thermoplastics materials. Therefore, while the company can only be held liable for the quality of delivered of virgin material, it is committed to supplying the information which will allow processors to achieve the levels of quality and performance expected by customers. GE Plastics recommends the use of a specific methodology wherever plastics are to be reground for reuse.

The recommended methodology to determine whether, and to what extent, reground materials can be used for the production of industrial products is as follows:

- define the critical characteristics and the acceptable level of performance in agreement with the final end-user
- conduct trials with different mixing levels of regrind, for example in steps of 10, 20, 30%, etc.
- measure the characteristics of the parts produced with these levels

- compare the obtained values with the acceptable level of performance and select accordingly
- agree with the end-user the maximum acceptable proportion of regrind



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\* A word of thanks for the permission to quote some phrases

\*\* A word of thanks for the permission to use pictures of mouldings with defects





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